

**AMENDMENTS TO THE CLAIMS**

1. (Currently amended) A process for hydrocracking a hydrocarbon feedstock into a low aromatic content middle distillate in the presence of hydrogen, comprising:

providing a catalyst comprising a catalyst support, the catalyst support comprising 1 to 15 wt% beta zeolite and [[a]] 1 to 15 wt% Y zeolite, at elevated temperature and pressure of 260-430° C and 5-20MPa, the Y zeolite having a unit cell size below 24.40 Å and a molar  $\text{SiO}_2:\text{Al}_2\text{O}_3$  ratio of at least 15, the beta zeolite having a silica-alumina ratio of at least about 250; and

contacting the feedstock with the catalyst in the presence of hydrogen at elevated temperature and pressure of 260-430° C and 5-20MPa, to obtain a middle distillate with a content of aromatic compounds and a pour point lower than the same fraction contained in the feedstock content.

2. (Original) The process of claim 1, wherein the Y zeolite has a unit cell size below 24.30 Å.

3. (Original) The process of claim 1, wherein the hydrocracking catalyst composition further comprises one or more hydrogenation components selected from nickel, cobalt, molybdenum, tungsten and chromium, their oxides and sulphides.

4. (Original) The process of claim 3 wherein the hydrogenation component is selected from nickel and tungsten, their oxides and sulphides.

5. (Original) The process of claim 1, wherein the said catalyst composition further comprises at least one amorphous component selected from the group comprising silica, alumina, titania, zirconium and their binary and tertiary compounds.

6. (Original) The process of claim 1, wherein the catalyst is in form of a physical mixture of beta zeolite and Y zeolite particles.

7. (Previously presented) The process of claim 1, in which the hydrocarbon feedstock has been subjected to hydrotreating so as to reduce its organic nitrogen and sulphur content.